Joint Crediting Mechanism Approved Methodology VN_AM009 "Installation of Container Formation Facility at Lead Acid Battery Factory"

A. Title of the methodology

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Installation of Container Formation Facility at Lead Acid Battery Factory, Version 01.10

B. Terms and definitions

Terms	Definitions	
container formation	A formation method of lead acid battery in which the battery	
	is assembled with non-converted plates and then converted in	
	the container.	
container formation facility	A facility in which container formation of lead acid battery is	
	done. Two processes of tank formation (formation and	
	charging) are integrated into this facility. Drying facility in	
	tank formation is no longer needed in container formation.	
tank formation	A formation method of lead acid battery in which the plates	
	are converted in a formation tank after being manufactured	
	and then assembled into a battery.	
tank formation facilities	Facilities including "formation tank" and "washing facility"	
	at tank formation process, "drying facility" at plate drying	
	process, and "charging facility" at charging process.	

C. Summary of the methodology

Items	Summary	
GHG emission reduction	Installation of container formation facility at lead acid battery	
measures	production line in place of tank formation facilities leads to	
	reduction of electricity and fossil fuel consumption by the	
	production line.	
Calculation of reference	Reference emissions from electricity consumption are calculated	
emissions	by multiplying electricity consumption of reference tank	

	formation facilities and CO ₂ emission factor for electricity
	consumed.
	Electricity consumption of reference tank formation facilities is
	calculated with production output of lead acid battery and
	specific electricity consumption by the reference facilities.
	Reference emissions from fuel consumption are calculated by
	multiplying net heat quantity required for fuel consumption to
	produce lead acid battery by reference tank formation facilities
	and CO ₂ emission factor.
	Net heat quantity required for fuel consumption to produce lead
	acid battery by reference tank formation facilities is calculated
	with production output of lead acid battery and specific net heat
	quantity required for fuel consumption per lead acid battery by
	the reference facilities.
Calculation of project	Project emissions are calculated by multiplying electricity
emissions	consumption of project container formation facility including
	chillier and cooling tower and CO_2 emission factor for
	electricity consumed.
Monitoring parameters	• Production output of lead acid battery at the container
	formation facility in the project factory per lead acid
	battery type
	• Capacity of lead acid battery
	• Electricity consumption by the container formation facility
	including chillier and cooling tower in the project factory

D. Eligibility criteria				
This methodology is applicable to projects that satisfy all of the following criteria.				
Criterion 1	Container formation facility is newly installed or installed to replace tank			
	formation facilities at lead acid battery production line.			

E. Emission Sources and GHG types

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Reference emissions		
Emission sources	GHG types	

Electricity consumption by tank formation facilities	CO ₂	
Fossil fuel (LPG) consumption by tank formation facilities	CO ₂	
Project emissions		
Emission sources	GHG types	
Electricity consumption by container formation facility	CO ₂	
Electricity consumption by cooling chiller and cooling tower	CO ₂	

F. Establishment and calculation of reference emissions

F.1. Establishment of reference emissions

Electricity and fossil fuel are consumed for the process of producing lead acid batteries in tank formation facilities.

Reference emissions from electricity consumption are calculated by multiplying specific electricity consumption per unit of lead acid battery type i (*SEC*_{*RE,i*}) [kWh/unit], production output of lead acid battery type i [units/p], and CO₂ emission factor for electricity consumed [tCO₂/MWh].

Reference emissions from fuel consumption are calculated by multiplying specific net heat quantity required for fuel consumption per unit of lead acid battery type i (*SNHQ*_{*RE,i*}) [MJ/unit], production output of lead acid battery type i [units/period] and CO₂ emission factor for fuel which is determined as per a factory where a JCM project is implemented [tCO₂/GJ].

In this methodology, SEC_{RE} is calculated with the equation specified, which is formulated in a conservative manner by excluding the electricity consumption by chiller and cooling tower to achieve net emission reductions while typical configuration of the equipment for producing lead acid batteries in tank formation facilities consists of the followings: formation tank, charging facility, chiller and cooling tower and other tank formation facilities such as washing facility and/or drying facility.

F.2. Calculation of reference emissions

$$RE_{p} = \sum_{k} \left[\left(EC_{RE,k,p} \times EF_{elec,k} \right) + \left(NHQ_{RE,k,p} \times EF_{fuel,k} \right) \right]$$

$\begin{split} & \mathcal{N}HQ_{RE,k,p} = \sum_{l} \left(SNHQ_{RE,l,k} \times N_{l,k,p} \right) \times \frac{1}{1,000} \\ & SEC_{RE,l,k} = 0.1338 \times AH_{l} + 0.1531 \\ & SNHQ_{RE,l,k} = 0.3282 \times AH_{l} + 0.9377 \end{split}$		$EC_{RE,k,p} = \sum_{i} \left(SEC_{RE,i,k} \times N_{i,k,p} \right) \times \frac{1}{1,000}$
$SNHQ_{RE,i,k} = 0.3282 \times AH_i + 0.9377$ $Where$ $RE_p \qquad Reference emissions during the period p [tCO_2/p] \\ EC_{RE,k,p} \qquad Electricity consumption by tank formation facilities in the project factory k during the period p [MWh/p] \\ EF_{elec,k} \qquad CO_2 emission factor for electricity consumed in the project factory k [tCO_2/MWh] \\ NHQ_{RE,k,p} \qquad Net heat quantity required for fuel consumption to produce lead acid battery by tank formation facilities in the project factory k [tCO_2/GJ] \\ SEC_{RE,i,k} \qquad Specific electricity consumption per lead acid battery type i by the reference facilities in the project factory k [tCO_2/GJ] \\ SEV_{RE,i,k} \qquad Specific net heat quantity required for fuel consumption per lead acid battery type i by the reference facilities in the project factory k [tM/unit] \\ NHQ_{RE,i,k} \qquad Specific net fact quantity required for fuel consumption per lead acid battery type i by the reference facilities in the project factory k [tM/unit] \\ Ni_{k,p} \qquad Specific net heat quantity required for fuel consumption per lead acid battery type i by the reference facilities in the project factory k [tM/unit] \\ Ni_{k,p} \qquad Production output of lead acid battery type i in the project factory k during the project factory k [tM/unit] \\ Ni_{k,p} \qquad Production output of lead acid battery type i in the project factory k during the project factory k during the project factory k [tM-j_1] \\ i \qquad Gapacity of lead acid battery type i [Ah/unit] \\ KHP_{k,k} \qquad Specific number of the project lead acid battery type i by the reference facilities in the project factory k [tM-j_1] \\ KHP_{k,k} \qquad Specific number of the project lead acid battery type i in the project factory k during the period p [totic] \\ KHP_{k,k} \qquad Specific number of the project lead acid battery type i] \\ KHP_{k,k} \qquad Specific number of the project factory k [tM-j_1] \\ KHP_{k,k} \qquad Specific number of the project factory k [tM$		$NHQ_{RE,k,p} = \sum_{i} (SNHQ_{RE,i,k} \times N_{i,k,p}) \times \frac{1}{1,000}$
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	AH _i	Capacity of lead acid battery type i [Ah/unit]
<i>k</i> Identification number of the project factory	i	Identification number of the project lead acid battery type
	k	Identification number of the project factory

G. Calculation of project emissions

$$PE_p = \sum_{k} (EC_{PJ,k,p} \times EF_{elec,k})$$

Where

PE_p	Project emissions during the period p [tCO ₂ /p]
$EC_{PJ,k,p}$	Electricity consumption by the container formation facilities including chillier
	and cooling tower in the project factory k during the period p [MWh/p]

 $EF_{elec,k}$ CO_2 emission factor for electricity consumed in the project factory k
[tCO2/MWh]kIdentification number of the project factory

H. Calculation of emissions reductions

$$ER_p = RE_p - PE_p$$

Where

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ER_p	Emission reductions during the period p [tCO ₂ /p]
RE_p	Reference emissions during the period p [tCO ₂ /p]
PE_p	Project emissions during the period $p [tCO_2/p]$

I. Data and parameters fixed *ex ante*

The source of each data and parameter fixed *ex ante* is listed as below.

Parameter	Description of data	Source
EF _{elec,k}	CO ₂ emission factor for consumed electricity	[Grid electricity]
	in the project factory k	Ministry of Natural Resources
		and Environment (MONRE),
	When project container formation facility	Vietnamese DNA for CDM
	consumes only grid electricity or captive	unless otherwise instructed by
	electricity, the project participant applies the	the Joint Committee.
	CO ₂ emission factor respectively.	
		[Captive electricity]
	When project container formation facility may	For the option a)
	consume both grid electricity and captive	Specification of the captive
	electricity, the project participant applies the	power generation system in the
	CO ₂ emission factor with lower value.	project factory k provided by
		the manufacturer $(\eta_{elec,CG,k} [\%])$.
	[CO ₂ emission factor]	CO ₂ emission factor of the
	For grid electricity: The most recent value	fossil fuel type used in the

available from the source stated in this table at cap the time of validation sys

For captive electricity, it is determined based on the following options:

a) Calculated from its power generation
efficiency in the project factory *k* (η_{elec,CG,k}
[%]) obtained from manufacturer's
specification

The power generation efficiency based on lower heating value (LHV) of the captive power generation system from the manufacturer's specification is applied;

 $EF_{elec,k} = 3.6 \times \frac{100}{\eta_{elec,CG,k}} \times EF_{fuel,CG,k}$

b) Calculated from measured data The power generation efficiency calculated from monitored data of the amount of fuel input for power generation (FC_{PJ,CG,k,p}) and the amount of electricity generated (EG_{PJ,CG,k,p}) in the project factory *k* during the monitoring period *p* is applied. The measurement is conducted with the monitoring equipment to which calibration certificate is issued by an entity accredited under national/international standards;

$$EF_{elec,k} = FC_{PJ,CG,k,p} \times NCV_{fuel,CG,k}$$

$$\times FE$$
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 $\times EF_{\text{fuel,CG,k}} \times \frac{}{EG_{\text{PJ,CG,k,p}}}$

Where:

 $\text{NCV}_{\text{fuel},\text{CG},k}$: Net calorific value of fuel consumed by the captive power generation system in the project factory *k* [GJ/mass or volume] captive power generation system in the project factory k(EF_{fuel,CG,k} [tCO₂/GJ])

For the option b)

Generated and supplied electricity by the captive power generation system in the project factory k (EG_{PJ,CG,k,p} [MWh/p]). Fuel amount consumed by the captive power generation system in the project factory k(FC_{PJ,CG,k,p} [mass or volume/p]). Net calorific value (NCV_{fuel,CG,k} [GJ/mass or volume]) and CO₂ emission factor (EF_{fuel,CG,k} $[tCO_2/GJ])$ of the fuel consumed by the captive power generation system in the project factory k in order of preference: 1) values provided by the fuel supplier;

2) measurement by the project participants;

3) regional or national default values;

4) IPCC default values provided in tables 1.2 and 1.4 of Ch.1 Vol.2 of 2006 IPCC Guidelines on National GHG Inventories. Lower value is applied.

[Captive electricity with diesel fuel] CDM approved small scale methodology: AMS-I.A.

	Note:			
	In case the captive electricity generation			[Captive electricity with natural
	system meets all of the following conditions,			gas]
	the value in the following table may be			2006 IPCC Guidelines on
	applied to EF _{elec}	_{c,k} depending	on the consumed	National GHG Inventories for
	fuel type.			the source of EF of natural gas.
				CDM Methodological tool
	• The system	n is non-renev	vable generation	"Determining the baseline
	system			efficiency of thermal or electric
	• Electricity	generation ca	pacity of the	energy generation systems
	system is le	ess than or eq	ual to 15 MW	version02.0" for the default
				efficiency for off-grid power
	fuel type	Diesel fuel	Natural gas	plants.
	EF _{elec,k}	0.8 *1	0.46 *2	
	*1 The most rec	cent value at t	he time of	
	validation is app	plied.		
	*2 The value is calculated with the equation in			
	the option a) above. The lower value of default			
	effective CO ₂ emission factor for natural gas			
	(0.0543 tCO ₂ /G	J), and the m	ost efficient value	
	of default efficie	ency for off-g	grid gas turbine	
	systems (42%)	are applied.		
EF _{fuel,k}	CO ₂ emission fa	actor for fuel	applicable to the	Country specific data or IPCC
	project factory	$k [tCO_2/GJ]$		default value from "2006 IPCC
				Guidelines for National
	In case tank for	mation facilit	ies exist in the	Greenhouse Gas Inventory".
	project factory prior to the project			Lower limit value of the default
	implementation	, the lowest C	CO ₂ emission	net calorific value is applied.
	factor of the fuel used by the facilities may be			

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Otherwise, CO₂ emission factor for Natural

applied.

Gas is applied.

History of the document

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Version	Date	Contents revised
<u>01.1</u>	<u>19 January 2018</u>	 <u>Deleted unnecessary parameters in the tables for</u> <u>calculation of reference emissions and project emissions in</u> <u>MPS (input_separate) sheet of the Monitoring</u> <u>Spreadsheet ; and</u> <u>Modified the descriptions of the parameters "RE_i,p" and</u> <u>"PE_i,p" in MPS (input_separate) sheet of the Monitoring</u> Spreadsheet,
01.0	10 October 2017	JC6, Annex 4 Initial approval.