JCM Proposed Methodology Form

Cover sheet of the Proposed Methodology Form

Form for submitting the proposed methodology

Host Country	Socialist Republic of Viet Nam	
Name of the methodology proponents	YUASA TRADING CO., LTD.	
submitting this form		
Sectoral scope(s) to which the Proposed	3. Energy demand	
Methodology applies		
Title of the proposed methodology, and	Introduction of Non-Inverter Type High	
version number	Efficiency Centrifugal Chiller, Version 01.0	
List of documents to be attached to this form		
(please check):	⊠Additional information	
Date of completion	03/09/2019	

History of the proposed methodology

Version	Date	Contents revised
1.0	03/09/2019	First edition

A. Title of the methodology

Introduction of Non-Inverter Type High Efficiency Centrifugal Chiller, Version 01.0

B. Terms and definitions

Terms	Definitions	
Centrifugal chiller	Chiller equipped with a centrifugal compressor.	
Inverter	Apparatus to control the speed of the compressor motor in	
	order to maintain the ambient temperature.	
Cooling capacity	Capability of individual chiller to remove heat. In this	
	methodology, "cooling capacity" is used to represent a	
	cooling capacity per a single chiller unit and not for a system	
	with multiple chiller units.	
Periodical check	Periodical investigation of chiller done by manufacturer or	
	agent who is authorized by the manufacturer, in order to	
	maintain chiller performance.	

C. Summary of the methodology

Items	Summary	
GHG emission reduction	High efficiency centrifugal chiller is introduced to save energy,	
measures	which leads to GHG emission reductions.	
Calculation of reference	Reference emissions are GHG emissions from using reference	
emissions	chiller, calculated with power consumption of project chiller,	
	ratio of COPs (Coefficient Of Performance) of reference/project	
	chillers and CO ₂ emission factor for electricity consumed.	
Calculation of project	Project emissions are GHG emissions from using project chiller,	
emissions	calculated with power consumption of project chiller and CO ₂	
	emission factor for electricity consumed.	
Monitoring parameters	Power consumption of project chiller	

D. Eligibility criteria

This methodology is applicable to projects that satisfy all of the following criteria.

Criterion 1	Project chiller is a non-Inverter type centrifugal chiller with a capacity which is				
	less than or equals to 1,500 USRt.				
	* 1 USRt = 3.52 kW				
Criterion 2			lar i calculated	under the standa	rdizing temperature
Cinterion 2	1				
					ues set in the tables
	below. ("x" in the t	abie	represents cooling	capacity per unit.)	
	rm 1 11 COD		6		
	[Threshold COP va		for project chiller		
	Cooling capacity punit (USRt)	er	300≤x≤700	700 <x≤1,100< th=""><th>1,100<x≤1,500< th=""></x≤1,500<></th></x≤1,100<>	1,100 <x≤1,500< th=""></x≤1,500<>
	Threshold COP va	lua	5.67	5.87	6.05
	Threshold COF va	iue	3.07	3.67	0.03
					_
	COP _{PJ,tc,i} is calcula	ted b	by altering the tem	perature condition	as of COP of project
	chiller i (COP _{PJ,i})	froi	n the project spe	ecific conditions t	o the standardizing
	conditions. COP _{PJ,i} is derived from specifications prepared for the quotation or				
	factory acceptance	test (data by manufactur	rer.	
	[equation to calculate COP _{PJ,tc,i}]				
	$COP_{PJ,tc,i} = COP_{PJ,i} \times [(T_{cooling-out,i} - T_{chilled-out,i} + TD_{chilled} + TD_{cooling})$				
	$\div (37 - 7 + TD_{chilled} + TD_{cooling})]$				
	$COP_{PJ,tc,i}$	CO	P of project chiller	<i>i</i> calculated under	the standardizing
	temperature conditions* [-]				
	$COP_{PJ,i}$: COP of project chiller i under the project specific conditions				
	[-]				
	$T_{\text{cooling-out,i}}$: Output cooling water temperature of project chiller i set				
		und	ler the project spec	ific conditions [de	gree Celsius]
	$T_{\text{chilled-out,i}}$: Output chilled water temperature of project chiller i set				
	under the project specific conditions [degree Celsius]				
	TD _{cooling} : Temperature difference between condensing temperature				
	of refrigerant and output cooling water temperature:				
	1.5 degrees Celsius set as a default value [degree Celsius]				
	TD _{chilled} : Temperature difference between evaporating temperature				
	of refrigerant and output chilled water temperature:				
	1.5 degrees Celsius set as a default value [degree Celsius]				
	*The standardizing temperature conditions to calculate COP _{PJ,tc,i}				

	Chilled water: output 7 degrees Celsius	
	input 12 degrees Celsius	
	Cooling water: output 37 degrees Celsius	
	input 32 degrees Celsius	
Criterion 3	Periodical check is planned more than one (1) time annually.	
Criterion 4	Ozone Depletion Potential (ODP) of the refrigerant used for project chiller is	
	zero.	
Criterion 5	A plan for prevention of releasing refrigerant used for project chiller is prepared.	
	In the case of replacing the existing chiller with the project chiller, a plan for	
	prevention of releasing refrigerant used in the existing chiller to the air (e.g.	
	re-use the pure refrigerants and/or recover and destroy blend refrigerants) is	
	prepared. Execution of this plan is checked at the time of verification, in order to	
	confirm that refrigerant used for the existing one replaced by the project is	
	prevented from being released to the air.	

E. Emission Sources and GHG types

Reference emissions			
Emission sources	GHG types		
Power consumption by reference chiller CO ₂			
Project emissions			
Emission sources	GHG types		
Power consumption by project chiller	CO_2		

F. Establishment and calculation of reference emissions

F.1. Establishment of reference emissions

Reference emissions are calculated by multiplying power consumption of project chiller, ratio of COPs for reference/project chillers, and CO₂ emission factor for electricity consumed.

The COP of reference chiller is conservatively set as a default value in the following manner to ensure the net emission reductions.

- 1. The COP value tends to increase as the cooling capacity becomes larger.
- 2. The reference COP value varies by its cooling capacity.
- 3. The maximum values of COP in each cooling capacity range set for this methodology are defined as $COP_{RE,i}$ as described in Section I.

F.2. Calculation of reference emissions

$$\begin{split} RE_p &= \sum_i \{ EC_{PJ,i,p} \times \left(COP_{PJ,tc,i} \div COP_{RE,i} \right) \times EF_{elec} \} \\ COP_{PJ,tc,i} &= COP_{PJ,i} \times \left[(T_{cooling-out,i} - T_{chilled-out,i} + TD_{chilled} + TD_{cooling}) \right. \\ & \left. \div \left(37 - 7 + TD_{chilled} + TD_{cooling} \right) \right] \end{split}$$

Where

 RE_p Reference emissions during the period p [tCO₂/p]

 $EC_{PJ,i,p}$ Power consumption of project chiller i during the period p [MWh/p] $COP_{PJ,tc,i}$ COP of project chiller i calculated under the standardizing temperature

conditions [-]

 $COP_{RE,i}$ COP of reference chiller i under the standardizing temperature conditions [-]

EF_{elec} CO₂ emission factor for consumed electricity [tCO₂/MWh]

 COP_{PLi} COP of project chiller i under the project specific conditions [-]

 $T_{cooling-out,i}$ Output cooling water temperature of project chiller i set under the project

specific conditions [degree Celsius]

 $T_{chilled-out,i}$ Output chilled water temperature of project chiller i set under the project

specific conditions [degree Celsius]

 $TD_{cooling}$ Temperature difference between condensing temperature of refrigerant and

output cooling water temperature, 1.5 degrees Celsius set as a default value

[degree Celsius]

TD_{chilled} Temperature difference between evaporating temperature of refrigerant and

output chilled water temperature, 1.5 degrees Celsius set as a default value

[degree Celsius]

i Identification number of project chiller

G. Calculation of project emissions

$$PE_p = \sum_{i} (EC_{PJ,i,p} \times EF_{elec})$$

Where

 PE_p Project emissions during the period p [tCO₂/p]

$EC_{PJ,i,p}$	Power consumption of project chiller i during the period p [MWh/p]
EF_{elec}	CO ₂ emission factor for consumed electricity [tCO ₂ /MWh]

H. Calculation of emissions reductions

$\mathbf{ER_p} = \mathbf{RE_p} - \mathbf{PE_p}$				
Where				
ER_p	Emission reductions during the period p [tCO ₂ /p]			
RE_p	Reference emissions during the period p [tCO ₂ /p]			
PE_p	Project emissions during the period p [tCO ₂ /p]			

I. Data and parameters fixed ex ante

The source of each data and parameter fixed ex ante is listed as below.

Parameter	Description of data	Source
EF _{elec}	CO ₂ emission factor for consumed electricity.	[Grid electricity]
		Ministry of Natural
	When project chiller consumes only grid	Resources and Environment
	electricity or captive electricity generated by	of Vietnam (MONRE),
	fossil fuel, the project participant applies the CO ₂	Vietnamese DNA for CDM
	emission factor respectively.	unless otherwise instructed
		by the Joint Committee.
	When project chiller may consume all or two of	
	the three electricity types (grid, captive by fossil	[Captive electricity]
	fuel, and captive by renewable energy), the	For the option a)
	project participant applies the grid CO ₂ emission	Specification of the captive
	factor for consumed grid electricity and the	power generation system
	captive CO ₂ emission factor for consumed	provided by the manufacturer
	captive electricity generated by fossil fuel and	(η _{elec,CG} [%]).
	renewable energy.	CO ₂ emission factor of the
		fossil fuel type used in the
	[CO ₂ emission factor]	captive power generation

(1) For grid electricity

The most recent value available from the source stated in this table at the time of validation is applied.

(2) For captive electricity

If the amount of electricity generated by renewable energy sources estimated from their generation capacities is equal to or less than half of the total electricity consumption at the project site, the captive CO₂ emission factor is determined from the following options using the data of fossil fuel generation only by option(a) or option(b).

If the amount is more than half, the CO₂ emission factor is determined by option (b) using total of the amount of electricity generated by both fossil fuel and renewable sources for EG_{PJ,CG,p}.

Option (a) Calculated from its power generation efficiency (η_{elec,CG} [%]) obtained from manufacturer's specification

The power generation efficiency based on lower heating value (LHV) of the captive power generation system from the manufacturer's specification is applied;

$$EF_{elec} = 3.6 \times \frac{100}{\eta_{elec,CG}} \times EF_{fuel,CG}$$

Option (b) Calculated from measured data
The power generation efficiency calculated from monitored data of the amount of fuel input for power generation (FC_{PJ,CG,p}) and the amount of electricity generated (EG_{PJ,CG,p}) during the monitoring period *p* is applied. FC_{PJ,CG,p} includes the amount of fossil fuel input only but does not include renewable energy. The amount of

system (EF_{fuel,CG} [tCO₂/GJ])

For the option b)

Generated and supplied electricity by the captive power generation system (EG_{PJ,CG,p} [MWh/p]).

Fuel amount consumed by the captive power generation system (FC_{PJ,CG,p} [mass or volume/p]).

Net calorific value $(NCV_{fuel,CG})$ [GJ/mass volume]) and CO₂ emission factor ($EF_{fuel,CG}$ [tCO_2/GJ]) of the fuel consumed by the generation captive power system in order of preference:

- 1) values provided by the fuel supplier;
- 2) measurement by the project participants;
- regional or national default values;
- 4) IPCC default values provided in tables 1.2 and 1.4 of Ch.1 Vol.2 of 2006 IPCC Guidelines on National GHG Inventories. Lower value is applied.

[Captive electricity with diesel fuel]
CDM approved small scale methodology: AMS-I.A.

electricity generated includes both by fossil fuel and renewable energy when necessary.

The measurement is conducted with the monitoring equipment to which calibration certificate is issued by an entity accredited under national/international standards;

$$\begin{split} EF_{elec} &= FC_{PJ,CG,p} \times NCV_{fuel,CG} \times EF_{fuel,CG} \\ &\times \frac{1}{EG_{PJ,CG,p}} \end{split}$$

Where:

 $NCV_{fuel,CG}$: Net calorific value of fuel consumed by the captive power generation system [GJ/mass or volume]

Note:

In case the captive electricity generation system meets all of the following conditions, the value in the following table may be applied to EF_{elec} depending on the consumed fuel type.

- The system is non-renewable generation system
- Electricity generation capacity of the system is less than or equal to 15 MW

fuel type	Diesel fuel	Natural gas
EF _{elec}	0.8*1	0.46*2

- *1 The most recent value at the time of validation is applied.
- *2 The value is calculated with the equation in the option (a) above. The lower value of default effective CO₂ emission factor for natural gas (0.0543 tCO₂/GJ), and the most efficient value of default efficiency for off-grid gas turbine systems (42%) are applied.

[Captive electricity with natural gas] 2006 IPCC Guidelines on National GHG Inventories for the source of EF of natural gas.

CDM Methodological tool
"Determining the baseline
efficiency of thermal or
electric energy generation
systems version02.0" for the
default efficiency for off-grid
power plants.

temperature conditions. The COP of the reference chiller <i>i</i> is selected from the default COP value in the following table in line with cooling capacity of the project chiller <i>i</i> . ("x" in the table represents cooling capacity per unit.) The COP values for reference chiller is unit (USR) and it (USR) and it (USR) are derived from the result of survey on COP of chillers from manufacturers that have high market share. The survey should prove the use of clear methodology. The default COP values should be revised if necessary from survey result which is conducted by JC or project participants. COP _{PJ,i} The COP of project chiller <i>i</i> under the project specific conditions. The COP of project chiller <i>i</i> under the project chiller <i>i</i> prepared for the quotation or factory acceptance test data by manufacturer The COP of project chiller <i>i</i> under the project chiller <i>i</i> prepared for the quotation or factory acceptance test data by manufacturer The COP of project chiller is et under the project specific conditions. The COP of project chiller is et under the project specific conditions. The COP of project chiller is et under the project specific conditions. The COP of project chiller is et under the project specific conditions. The COP of project chiller is et under the project specific conditions. The COP of project chiller is et under the project specific conditions. The COP of project chiller is et under the project specific conditions. The COP of project chiller is et under the project specific conditions.	$COP_{RE,i}$	COP of reference chiller i under the standardizing	Specifications of project
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