# ${\bf Joint\ Crediting\ Mechanism\ Approved\ Methodology\ ID\_AM009}$ "Replacement of conventional burners with regenerative burners for aluminum holding furnaces"

# A. Title of the methodology

Replacement of conventional burners with regenerative burners for aluminum holding furnaces, ver. 24.0

## B. Terms and definitions

Terms	Definitions
Regenerative burner	Burner systems which absorb exhaust gas heat to a reservoir and
	preheat combustion air using the absorbed heat in the reservoir to
	improve energy efficiency.
Conventional burner	Burner systems which do not have combustion air preheating facility.
Periodical check	Periodical investigation of furnace done by manufacturer or agent
	who is authorized by the manufacturer, in order to maintain furnace
	performance.

## C. Summary of the methodology

Items	Summary
GHG emission reduction	By replacing conventional burners with regenerative burners for
measures	aluminum holding furnaces, consumption of natural gas is
	reduced, which leads to the reduction of GHG emissions.
Calculation of reference	Reference emissions are the CO <sub>2</sub> emissions from the use of
emissions	reference burners in an aluminum holding furnace, which are
	calculated based on the consumption of natural gas in the
	project furnace and energy efficiency of the reference and
	project burners.
Calculation of project	Project emissions are the CO <sub>2</sub> emissions from the use of project
emissions	burners in an aluminum holding furnace, which are calculated
	based on the consumption of natural gas and electricity in the
	project furnace.

Items	Summary	
Monitoring parameters	- Consumption of natural gas by the project furnace	
	- The number of operating days	

## D. Eligibility criteria

This methodology is applicable to projects that satisfy all of the following criteria.

Criterion 1	The project replaces conventional burners with regenerative burners for	
	aluminum holding furnaces.	
Criterion 2	Holding temperature of aluminum melt, which is determined in the furnace	
	user's specification, is within the range from 600 to 800 degrees Celsius.	
Criterion 3	The regenerative burners have a structure which leads all exhaust gas to flow	
	through the heat reservoir before discharging it into the atmosphere.	
Criterion 4	Periodical check is planned at least once a year.	

## E. Emission Sources and GHG types

Reference emissions		
Emission sources	GHG types	
Combustion of natural gas in the reference furnace	$CO_2$	
Project emissions		
Emission sources GHG type		
Combustion of natural gas in the project furnace	CO <sub>2</sub>	
Power consumption by the project furnace CO <sub>2</sub>		

## F. Establishment and calculation of reference emissions

#### F.1. Establishment of reference emissions

The methodology results in conservative calculation of emission reductions and ensures net reduction of emissions by the following approaches:

#### 1. Setting energy efficiencies of burners in a conservative manner

It can be said that the energy efficiency of burners increases as the exhaust gas temperature falls (and vice versa), since high exhaust gas temperature means that heat is released without being used. In this methodology, the energy efficiencies are set as default values by assuming the

exhaust gas temperature conservatively.

For the reference burner, the exhaust gas temperature is set as 750 degrees Celsius. When the holding temperature is designed to be within the range from 600 to 800 degrees Celsius, the actual furnace atmospheric temperature is generally in the range of 750 to 950 degrees Celsius. Therefore, for the reference burner, the exhaust gas temperature is assumed to be equal to the lower end of furnace atmospheric temperature for the sake of conservativeness.

For the project burner, the exhaust gas temperature is set as 300 degrees Celsius. When the holding temperature is designed to be within the range from 600 to 800 degrees Celsius, the actual furnace atmospheric temperature is generally in the range of 750 to 950 degrees Celsius for project burner, too. In addition, for the project burner, the exhaust gas temperature is lower than the furnace atmospheric temperature due to the heat absorber; when the furnace atmospheric temperature is in the range of 750 to 950 degrees Celsius, the possible temperature of the project exhaust gas is less than 300 degrees Celsius. Therefore, for the project burner, the exhaust gas temperature is set as the upper end of the possible exhaust gas temperature for the sake of conservativeness.

Therefore, this methodology results in the conservative calculation of reference emissions by assuming the lower reference exhaust gas temperature and the higher project exhaust gas temperature in setting the burner efficiencies.

#### 2. Omitting reference power consumption

Although electricity is used in the reference furnace, CO<sub>2</sub> emissions from power consumption are not included in the reference emissions for the purpose of ensuring simplicity and conservativeness.

#### F.2. Calculation of reference emissions

Reference emissions are calculated as follows:

$$RE_{p} = \sum_{i} \{ FC_{PJ,NG,i,p} \times (\eta_{PJ,i} \div \eta_{RE,i}) \times NCV_{NG} \times EF_{NG} \}$$

Where:

RE<sub>p</sub> Reference emissions during the period p [tCO<sub>2</sub>/p]

FC<sub>PJ,NG,i,p</sub> Consumption of natural gas by the project furnace i during the period p [Nm<sup>3</sup>/p]

 $\eta_{PJ,i}$  Energy efficiency of the project burner of the project furnace i [-]

 $\eta_{RE,i}$  Energy efficiency of the reference burner of the project furnace i [-]

 $NCV_{NG}$  Net calorific value of natural gas [GJ/Nm<sup>3</sup>]  $EF_{NG}$   $CO_2$  emission factor of natural gas [tCO<sub>2</sub>/GJ]

#### G. Calculation of project emissions

Project emissions are calculated as follows:

$$PE_p = PE_{NG,p} + PE_{elec,p}$$

Where:

PE<sub>p</sub> Project emissions during the period p [tCO<sub>2</sub>/p]

PE<sub>NG,p</sub> Project emissions from natural gas consumption during the period p [tCO<sub>2</sub>/p] PE<sub>elec,p</sub> Project emissions from electricity consumption during the period p [tCO<sub>2</sub>/p]

$$PE_{NG,p} = \sum_{i} (FC_{PJ,NG,i,p} \times NCV_{NG} \times EF_{NG})$$

Where:

PE<sub>NG,p</sub> Project emissions from natural gas consumption during the period p [tCO<sub>2</sub>/p] FC<sub>PJ,NG,i,p</sub> Consumption of natural gas by the project furnace i during the period p [Nm<sup>3</sup>/p]

 $NCV_{NG}$  Net calorific value of natural gas [GJ/Nm<sup>3</sup>]  $EF_{NG}$   $CO_2$  emission factor of natural gas [tCO<sub>2</sub>/GJ]

$$PE_{elec,p} = EC_{PJ,p} \times EF_{elec}$$

Where:

PE<sub>elec,p</sub> Project emissions during the period p (from electricity) [tCO<sub>2</sub>/p]

 $EC_{PJ,p}$  Consumption of electricity by the project furnace during the period p [MWh/ p]

EF<sub>elec</sub> CO<sub>2</sub> emission factor for consumed electricity [tCO<sub>2</sub>/MWh]

$$EC_{PJ,p} = \sum_{i} \left\{ RC_{CAP,i} \times 10^{-6} \times 24(hours/day) \times D_{op,i,p} \right\}$$

Where:

 $EC_{PJ,p}$  Consumption of electricity by the project furnace during the period p [MWh/p]

 $RC_{CAP,i}$  The total maximum rated capacity of auxiliary equipment of the project furnace i

[W]

 $D_{op,i,p}$  The number of operating days of the project furnace i during the period p [day/p]

## H. Calculation of emissions reductions

Emissions reductions are calculated as follows:

 $ER_p = RE_p - PE_p$ 

Where:

 $\mathrm{ER}_{\mathrm{p}}$  Emissions reductions during the period p [tCO<sub>2</sub>/ p]  $\mathrm{RE}_{\mathrm{p}}$  Reference emissions during the period p [tCO<sub>2</sub>/ p]  $\mathrm{PE}_{\mathrm{p}}$  Project emissions during the period p [tCO<sub>2</sub>/ p]

## I. Data and parameters fixed ex ante

The source of each data and parameter fixed ex ante is listed as below.

Parameter	Description of data	Source	
$NCV_{NG}$	Net calorific value of natural gas	IPCC Special Report on Carbon	
	[GJ/Nm <sup>3</sup> ]	dioxide Capture and Storage, Annex	
	The IPCC value is converted by gas	I, Table AI.10. Lower Heating Value	
	composition and molecular weight.	(LHV) is applied.	
	The default value for $NCV_{NG}$ is set as		
	$0.036659 \text{ GJ/Nm}^3$ .		
EF <sub>NG</sub>	CO <sub>2</sub> emission factor of natural gas	Country specific data or IPCC default	
	[tCO <sub>2</sub> /GJ]	value from "2006 IPCC Guidelines	
		for National Greenhouse Gas	
		Inventory".	
		Lower limit value of the default CO <sub>2</sub>	
		emission factor is applied.	
$\eta_{RE,i}$	Energy efficiency of the reference burner	See explanatory note 1.	
	of the project furnace $i$ [-]		
	The default value for $\eta_{\text{RE}}$ is set as 0.682.		
$\eta_{\mathrm{PJ},i}$	Energy efficiency of the project burner of	See explanatory note 2.	
	the project furnace i [-]		

Parameter	Description of data	Source
	The project-specific value is calculated by	
	the equation in explanatory note 2 using	
	the recommended operational value of air	
	ratio in the manual of the project burner.	
m <sub>r</sub>	Air ratio for the reference burner	The recommended operational value
		in the manual of the project burner
	The same value as air ratio for the project	
	burner (m <sub>p</sub> ) is applied.	
$m_p$	Air ratio for the project burner	The recommended operational value
		in the manual of the project
	The recommended operational value in	<u>burner</u> See explanatory note 2.
	the manual of the project burner.	
EF <sub>elec</sub>	CO <sub>2</sub> emission factor for consumed	[Grid electricity]
	electricity.	The data is sourced from "Emission
	When the project furnace consumes only	Factors of Electricity Interconnection
	grid electricity or captive electricity, the	Systems", National Committee on
	project participant applies the CO <sub>2</sub>	Clean Development Mechanism
	emission factor respectively.	(Indonesian DNA for CDM), based
	When the project furnace may consume	on data obtained by Directorate
	both grid electricity and captive	General of Electricity, Ministry of
	electricity, the project participant applies	Energy and Mineral Resources,
	the CO <sub>2</sub> emission factor with lower value.	Indonesia, unless otherwise instructed
		by the Joint Committee.
	[CO <sub>2</sub> emission factor]	[Captive electricity]
	For grid electricity: The most recent value	CDM approved small scale
	available from the source stated in this	methodology AMS-I.A
	table at the time of validation	
	For captive electricity: 0.8* [tCO <sub>2</sub> /MWh]	
	*The most recent value available from	
	CDM approved small scale methodology	
	AMS-I.A at the time of validation is	
	applied.	
$RC_{CAP}$	The total maximum rated capacity of	Specification or nameplate of
	auxiliary equipment of the project furnace	auxiliary equipment of the project
	[W]	furnace

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$$\eta_{RE} = \quad \frac{NCV_{NG} \text{-} \left[Gw_{NG} * c_{1,r} * (T_{1,r} \text{-} T_2) + A_{0,NG} * (m_r \text{-} 1) * c_{2,r} * (T_{1,r} \text{-} T_2)\right]}{NCV_{NG}}$$

Where:

 $\eta_{RE}$  Energy efficiency of the reference burner [-]

NCV<sub>NG</sub> Net calorific value of natural gas: the default value for NCV<sub>NG</sub> is set as **36,659** [kJ/Nm<sup>3</sup>] based on *IPCC Special Report on Carbon dioxide Capture and Storage*, Annex I, Table AI.10, and it is converted by gas composition and molecular weight.

Gw<sub>NG</sub> Theoretical volume of wet exhaust gas from combustion of natural gas: the default value for  $Gw_{NG}$  is set as **10.694** [Nm<sup>3</sup>/Nm<sup>3</sup>] based on the assumed natural gas composition of  $CH_4$ : 94.4%,  $C_2H_6$ : 3.1%,  $C_8H_8$ : 0.5%, and  $C_4H_{10}$ : 0.2% based on *IPCC Special Report on Carbon dioxide Capture and Storage*, Annex I, Table AI.10.

Average specific heat at constant pressure of wet exhaust gas of natural gas, at the reference temperature of exhaust gas: the default value for  $c_{1,r}$  is set as 1.455 [kJ/Nm<sup>3</sup>·degree Celsius] based on the aforementioned natural gas composition and JIS G 0702, Appendix Table 2 (linear prediction is used for the estimation).

 $T_{1,r}$  Reference temperature of exhaust gas: the default value for  $T_{1,r}$  is set as **750** [degrees Celsius].

T<sub>2</sub> Ambient temperature (annual average in Jakarta): the default value for T<sub>2</sub> is set as **32.6** [degrees Celsius].

 $A_{0,NG}$  Theoretical amount of air of the natural gas: the default value for  $A_{0,NG}$  is set as **9.688** [Nm<sup>3</sup>/Nm<sup>3</sup>] based on the aforementioned natural gas composition.

 $m_r$  Air ratio for the reference burner: the same value as air ratio for the project burner  $(m_p)$  applied the default value for  $m_r$  is set as 1.05 in a conservative manner.

c<sub>2,r</sub> Average specific heat at constant pressure of air, at the reference temperature of exhaust gas: the default values for c<sub>2,r</sub> is set as **1.380** [kJ/ Nm<sup>3</sup>·degree Celsius] based on the aforementioned natural gas composition and JIS G 0702, Appendix Table 2 (Linear prediction is used for the estimation).

$$\eta_{\text{PJ}}\!=\!\frac{NCV_{NG}\text{-}\left[Gw_{NG}*c_{1,p}*(T_{1,p}\text{-}T_{2})+A_{0,NG}*(m_{p}\text{-}1)*c_{2,p}*(T_{1,p}\text{-}T_{2})\right]}{NCV_{NG}}$$

Where:

 $\eta_{PJ}$  Energy efficiency of the reference burner [-]

NCV<sub>NG</sub> Net calorific value of natural gas: the default value for NCV<sub>NG</sub> is set as **36,659** [kJ/Nm<sup>3</sup>] based on *IPCC Special Report on Carbon dioxide Capture and Storage*, Annex I, Table AI.10, and it is converted by gas composition and molecular weight.

Gw<sub>NG</sub> Theoretical volume of wet exhaust gas from combustion of natural gas: the default value for  $Gw_{NG}$  is set as **10.694** [Nm<sup>3</sup>/Nm<sup>3</sup>] based on the assumed natural gas composition of  $CH_4$ : 94.4%,  $C_2H_6$ : 3.1%,  $C_8H_8$ : 0.5%, and  $C_4H_{10}$ : 0.2% based on *IPCC Special Report on Carbon dioxide Capture and Storage*, Annex I, Table AI.10.

Average specific heat at constant pressure of wet exhaust gas of natural gas, at the project temperature of exhaust gas: the default value for  $c_{1,p}$  is set as **1.368** [kJ/Nm<sup>3</sup>·degree Celsius] based on the aforementioned natural gas composition and JIS G 0702, Appendix Table 2 (linear prediction is used for the estimation).

 $T_{1,p}$  Project temperature of exhaust gas: the default value for  $T_{1,p}$  is set as **300** [degrees Celsius].

T<sub>2</sub> Ambient temperature (annual average in Jakarta): the default value for T<sub>2</sub> is set as **32.6** [degrees Celsius].

 $A_{0,NG}$  Theoretical amount of air of the natural gas: the default value for  $A_{0,NG}$  is set as **9.688** [Nm<sup>3</sup>/Nm<sup>3</sup>] based on the aforementioned natural gas composition.

 $m_p$  Air ratio for the project burner: the recommended operational value in the manual of the project burner.

c<sub>2,p</sub> Average specific heat at constant pressure of air, at the *project* temperature of exhaust gas: the default values for c<sub>2,p</sub> is set as **1.319** [GJ/Nm<sup>3</sup>·degree Celsius] based on the aforementioned natural gas composition and JIS G 0702, Appendix Table 2 (Linear prediction is used for the estimation).

## History of the document

Version	Date	Contents revised
02.0	31 March 2016	Revisions to:  Change the description of air ratio for the reference burner (m <sub>r</sub> ) in Section I and Explanatory note 1; and Change the status of parameter "air ratio for the reference burner" from default value to a parameter fixed <i>ex ante</i> in

		the Monitoring Spreadsheet.
01.0	6 August 2015	Electronic decision by the Joint Committee
		Initial approval.